

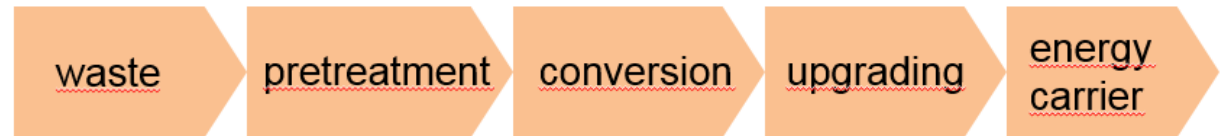
# Thermochemical Processes for Feedstock Recycling of Waste

Dieter Stapf, Helmut Seifert, Manuela Wexler

ABLC Global, San Francisco, November 7, 2018

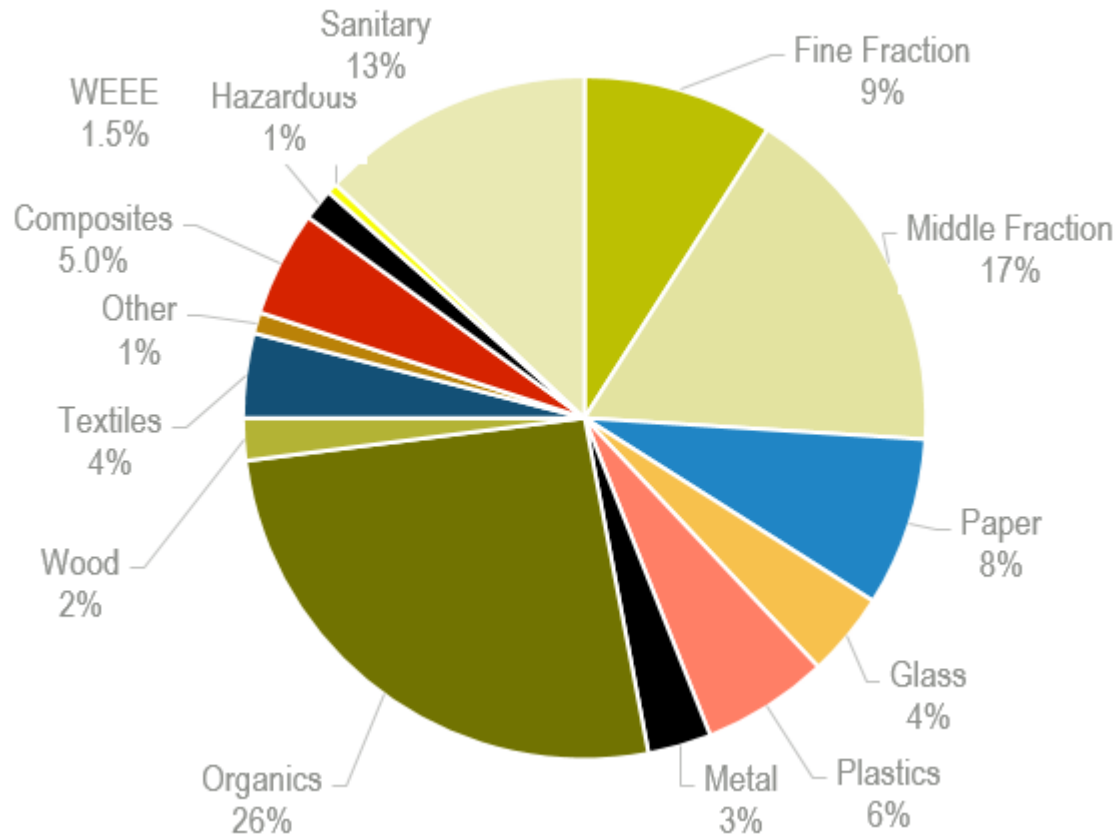


Certificated Solid Recovered Fuel (SRF) produced from biomass and household waste in the frame of the EU funded RECOMBIO project [1]



# Residual Household Waste Composition in Developed Countries

Average Composition RHW in Germany



Conversio, 2018, in: Survey on feedstock recycling of plastic waste (Publisher: BKV & plastics Europe, in prep.)

# Case: Residual Household Waste RHW to Methanol Syngas

## Feedstock Recycling of Waste

Pretreatment

Mechanical pretreatment

Conversion

Fluidized bed gasification

Product upgrading

Multi step syngas treatment

RHW



Gasifier Feed



Raw syngas

$\text{CO}_2$ ,  $\text{CO}$ ,  $\text{H}_2$ ,  $\text{CH}_4$ ,  
tars,  $\text{H}_2\text{S}$ ,  $\text{HCl}$ ,  
 $\text{Hg}$ , ...

On-spec-feed to methanol synthesis

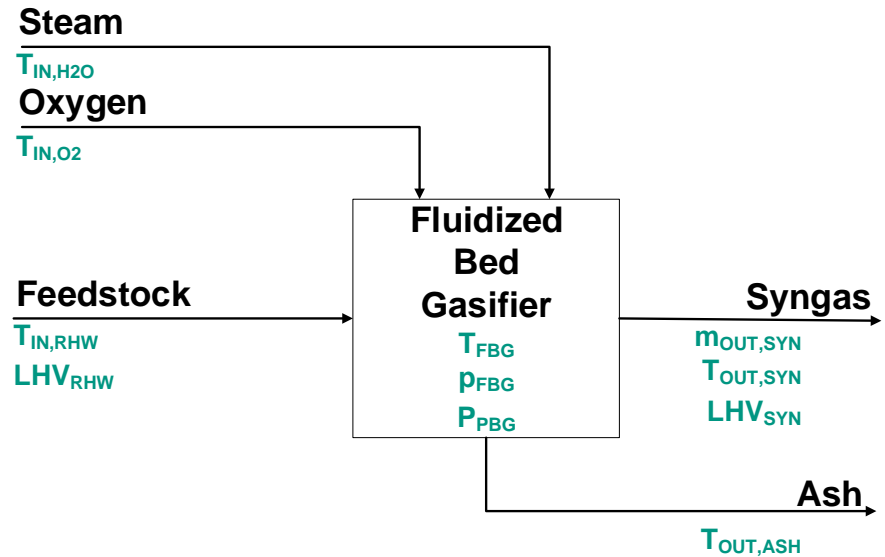
$\text{H}_2:\text{CO} = 2:1$ ,  
tar free, gas  
contaminants  
below 0.1ppmv

# CFB Gasification

# Gasification of RHW in a CFB-Gasifier

## Calculated Balance

- $T_{IN,RHW} = 25^{\circ}C$
- $T_{IN,O_2} = 23^{\circ}C$
- $T_{IN,H_2O} = 500^{\circ}C$
  
- $p_{CFB} = 1 \text{ bar}$
- $T_{OUT,SYN} = 950^{\circ}C$
- Input of  $O_2$



Syngas composition		
CO	mole-%	25.0
H <sub>2</sub>	mole-%	37.2
CO <sub>2</sub>	mole-%	15.3
H <sub>2</sub> O	mole-%	21.0
CH <sub>4</sub>	mole-%	0.08
O <sub>2</sub>	mole-%	0.00
N <sub>2</sub>	mole-%	1.1
H <sub>2</sub> : CO	/	1.488

Syngas composition		
LHV	MJ/m <sub>N</sub> <sup>3</sup>	7.2
Particles (Alkaline)	mg/m <sub>N</sub> <sup>3</sup>	
Tar	mg/m <sub>N</sub> <sup>3</sup>	10,000*
NH <sub>3</sub> / HCN	mg/m <sub>N</sub> <sup>3</sup>	16.5 / 0.0
H <sub>2</sub> S / COS	mg/m <sub>N</sub> <sup>3</sup>	992 / 2624
Halogenes (Cl, Br)	mg/m <sub>N</sub> <sup>3</sup>	
Heavy Metals	µg/m <sub>N</sub> <sup>3</sup>	

\*according to Han (2008)

# Gasification of RHW in a CFB-Gasifier

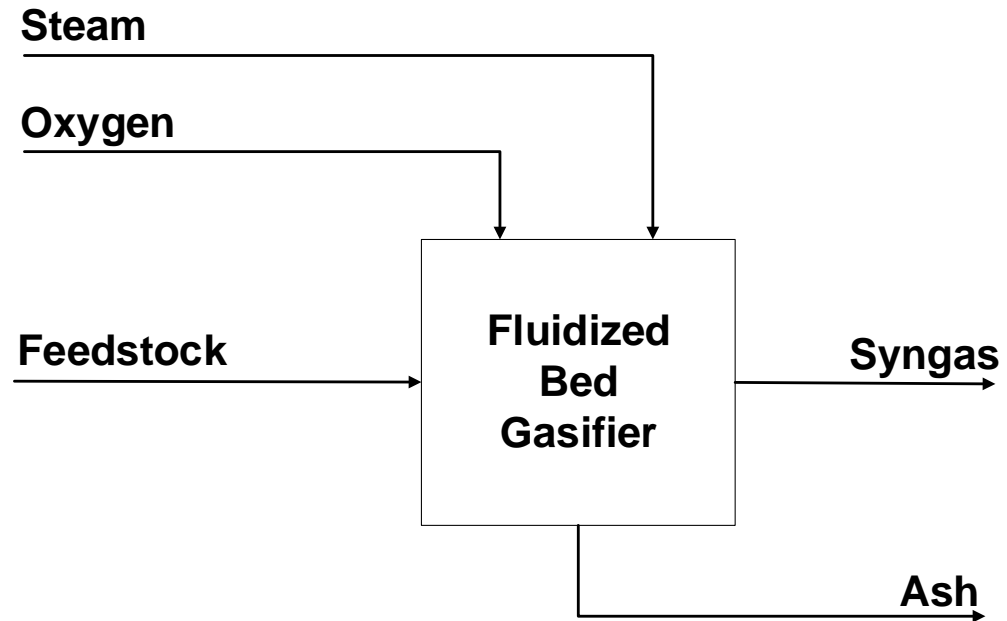
## Cost Calculation – Boundary Conditions

Thermal Capacity	[MW]	100
LHV <sub>Pretr.RHW</sub>	[MJ/kg]	15.0
→ Mass Flow Pretreated RHW	[t/h]	24.0

Temperature	[°C]	950
→ Mass Flow O <sub>2</sub>	[t/h]	10.2

Cold gas efficiency	[-]	> 0.8
→ Mass Flow H <sub>2</sub> O	[t/h]	3.6

Mass Flow Raw Gas	[t/h]	34.4
→ Volume Flow	[m <sub>N</sub> <sup>3</sup> /h]	41.208



### Further Assumptions

- O<sub>2</sub> has to be purchased
- Process heat is used to supply process steam (purchase of demin water)
- Combustion of Tars

# Gasification of RHW in a CFB-Gasifier

## Cost Calculation – CapEx & OpEx

Invest in 1995	[Mio. DM]	38.7	Scur (2001)
→ Invest in 2017	[Mio. €]	28.3	VCI (div.)

- Plant factor 3
- Annual costs of Gasifier:
  - Depreciation Period: 10 years
  - Depreciation: 10 % of Invest per year
  - Capital costs 10 % of Invest per year
  - Operating costs: 5 % of Invest per year

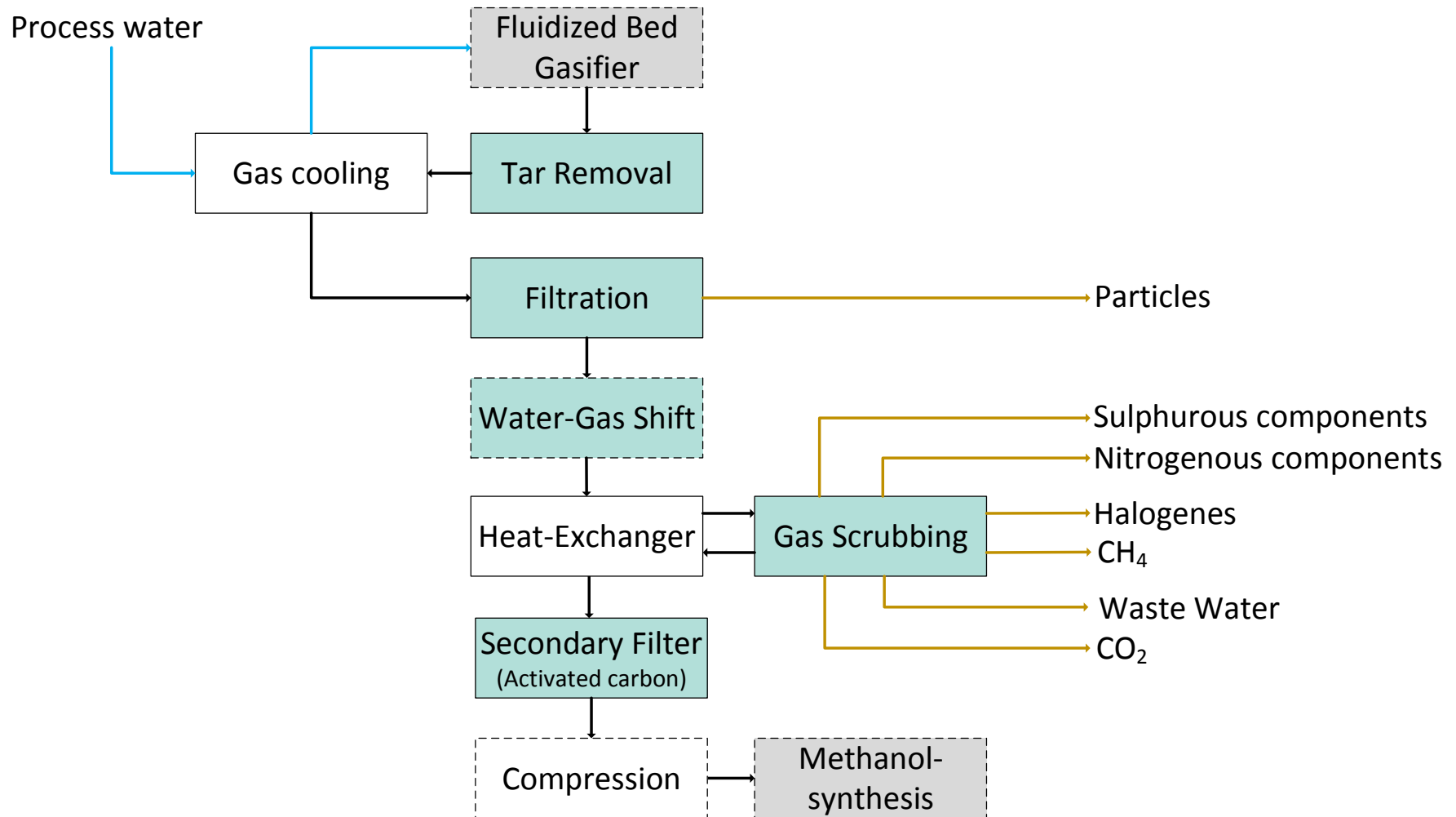
CapEx  
76 €/t<sub>RHW</sub>

Operation hours	[h/yr]	8,000	
Electricity	[MWh/h]	2.0	
	[€/kWh]	0.08	
Process Water	[€/t <sub>H2O</sub> ]	1.00	Doymaz (2015)
Oxygen	[€/t <sub>O2</sub> ]	19.00	Doymaz (2015)

OpEx  
10 €/t<sub>RHW</sub>

# Gasification of RHW in a CFB-Gasifier

## Gas conditioning – Flow scheme





# Gasification of RHW in a CFB-Gasifier

## Gas conditioning – Cost Calculation – CapEx & OpEx

### ■ Costs of main plant components [k€] (2017)

Tar Removal	6,562	Boerrigter (2015)
Heat Exchanger	249	Peters (2003)
Electrostatic Precipitator	683	Peters (2003) Scur (2001) CCA (2018)
Water-gas Shift	372	Trippe (2013)
Gas Scrubber (Rectisol)	10,618	Trippe (2013)
Activated Carbon Filter	20	gutmbh.de
Compressor	15.176	Peters (2003)

- Plant factor: 3
- Annual costs of Gas Cleaning Plant:
  - Depreciation Period: 10 years
  - Depreciation: 10 % of Invest/yr
  - Capital costs 10 % of Invest/yr
  - Operating costs: 5 % of Invest/yr

CapEx  
92 €/t<sub>RHW</sub>

### ■ Operating Parameters

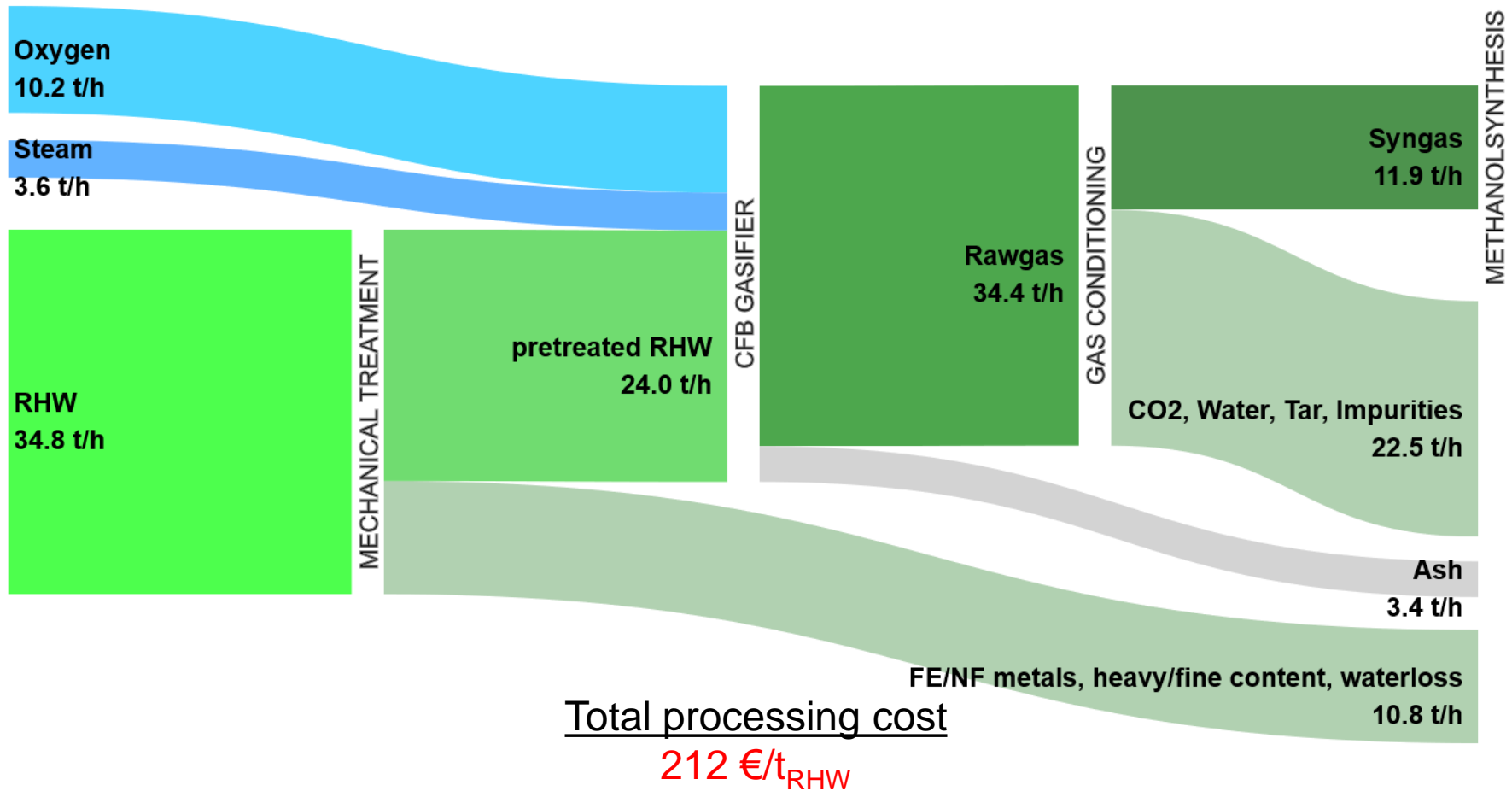
Operation hours	[h/yr]	8,000	
Electricity	[€/kWh]	0.08	
Waste Water	[€/t <sub>H2O</sub> ]	35.00	Messmer (2015)
Methanol	[€/t <sub>MeOH</sub> ]	367.50	Spitzbarth (2005)
CO <sub>2</sub> Emission	[€/t <sub>CO2</sub> ]	8	Doymaz (2015)
Activated Carbon	[€/t <sub>AC</sub> ]	2,000	gutmbh.de

- Ash is used as Feedstock in Cement Plant
- Tars are incinerated

OpEx  
13 €/t<sub>RHW</sub>

# Gasification of RHW in a CFB-Gasifier

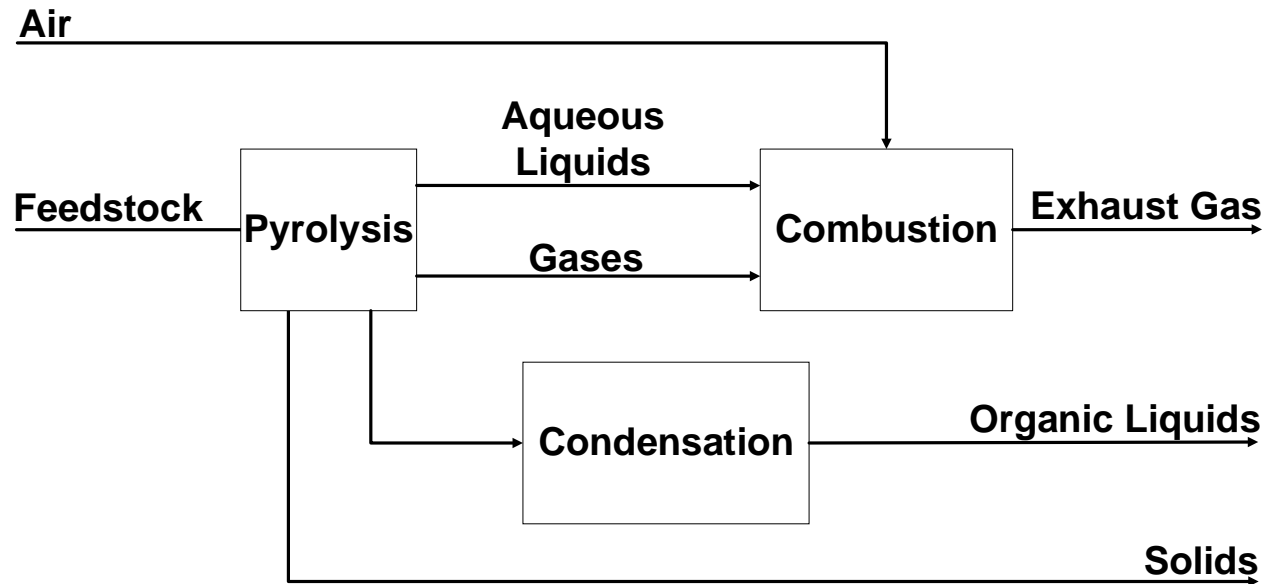
## Quantitative Evaluation of the Full Process Chain



# Pyrolysis

# Rotary Kiln Pyrolysis of RHW

## Cost Calculation – Boundary Conditions



Capacity Pyrolysis	[t/h]	22.4
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Temperature Exhaust Gas	[°C]	800
→ Mass Flow Air	[t/h]	90.3

Mass Flow Gases	[t/h]	4.1
Mass Flow Aqueous Liquids	[t/h]	7.2
Mass Flow Organic Liquids	[t/h]	5.6
Mass Flow Solids	[t/h]	5.5

# Rotary Kiln Pyrolysis of RHW

## Cost Calculation – CapEx & OpEx

### Costs of main plant components [Mio.€] (2017)

Total Rotary Kiln Pyrolysis plant	146.5	Based on Hartenstein 2004
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### Annual costs of Pyrolysis Plant:

- Depreciation Period: 10 years
- Depreciation: 10 % of Invest/yr
- Capital costs 10 % of Invest/yr
- Operating costs: 5 % of Invest/yr

### Operating Parameters

Process Heat		self-generated	
Combustion Air	[€/t]	4.17	Spitzbarth (2004)
Landfill Fees: solids	[€/t <sub>Solids</sub> ]	100	CCA (2018)
Revenue: District Heating	[€/kWh]	0.03	boerse.de

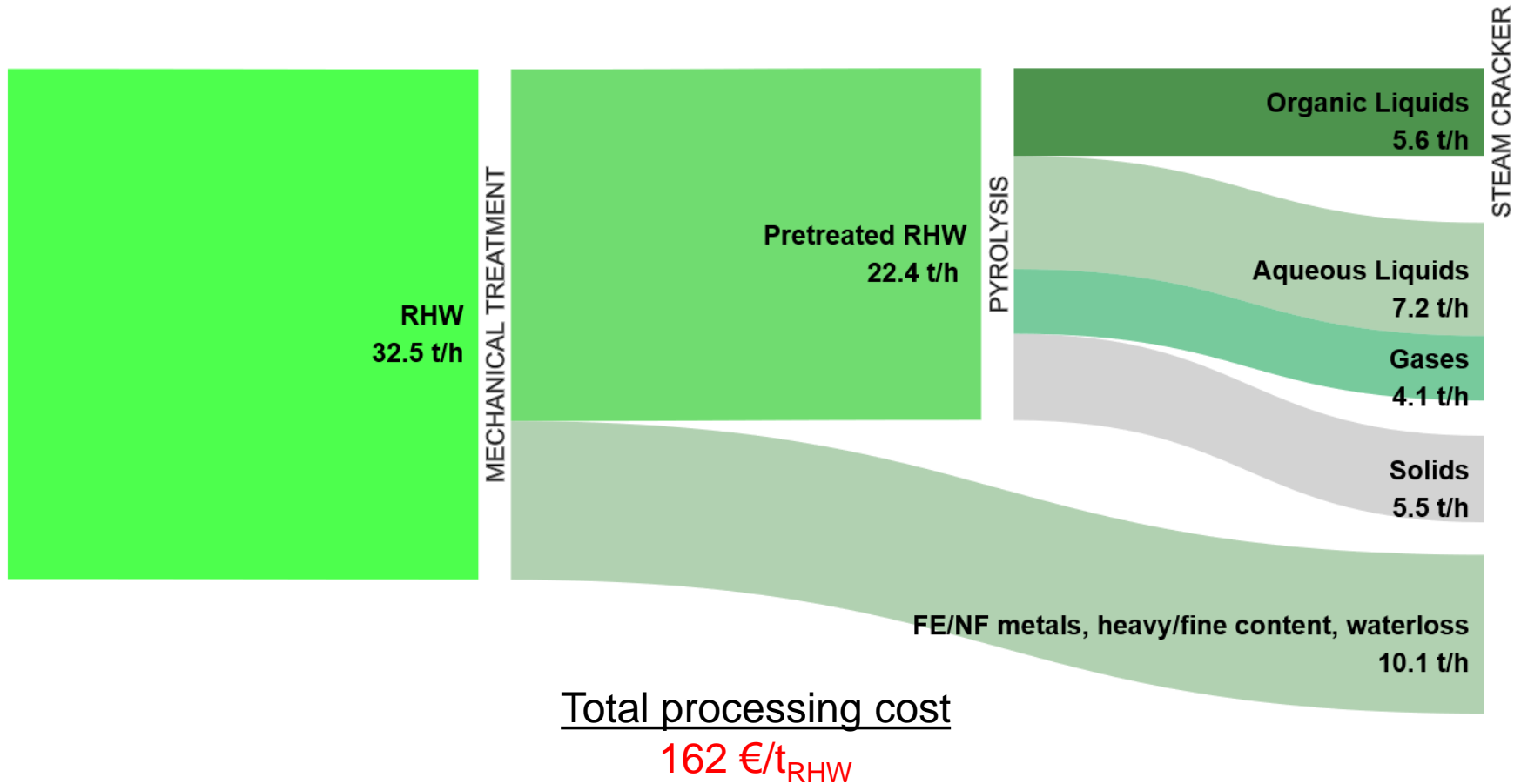
- Solids go to Landfill, class I
- Process heat is generated on side
- Excess Heat is sold as methane substitute (district heating grid)

CapEx  
141 €/t<sub>RHW</sub>

OpEx  
21 €/t<sub>RHW</sub>

# Rotary Kiln Pyrolysis of RHW

## Quantitative Evaluation of the Full Process Chain



# Summary

# Pyrolysis & Gasification Technology Readiness

Feedstock recycling of pretreated residual household waste

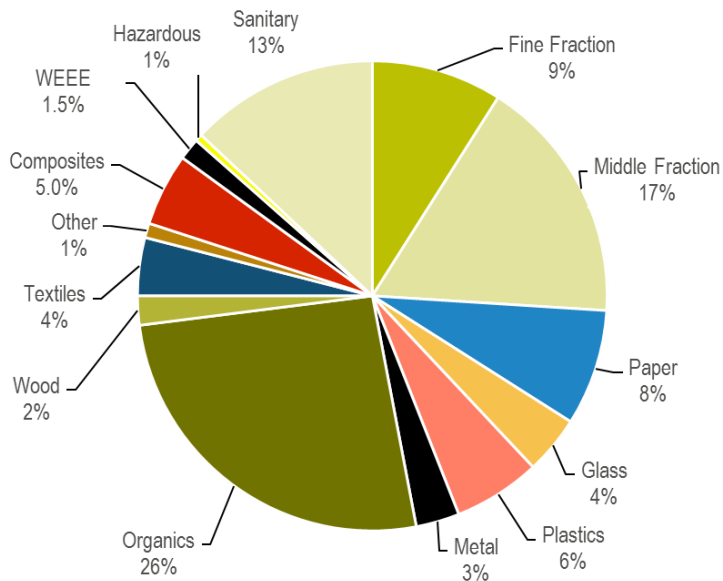
- CFB gasifier TRL: 8 - 9
  - Key technical issue:
    - Optimization and reliable operation of syngas postprocessing unit (Tar removal, plugging, etc.)
  
- Rotary kiln pyrolysis unit TRL: 5 - 6
  - Product composition and quality not validated
  - Key technical issues:
    - Design, optimization and reliable operation of a product condensing system (Plugging, polymerization, etc.)
    - Cost of pyrolysis product posttreatment systems
    - Optimization of a pyrolysis unit that assures multiproduct quality (organic condensate as cracker feedstock, solids quality) inline with required feedstock flexibility



# Process Overview: Economics\*\*

## Residual Household Waste (RHW)

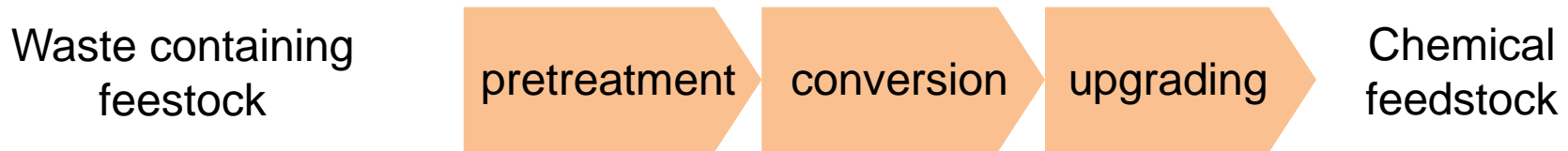
Process	Pretreatment [€/t <sub>RHW</sub> ]	Conversion [€/t <sub>RHW</sub> ]	Upgrading [€/t <sub>RHW</sub> ]	Total processing cost [€/t <sub>RHW</sub> ]	Revenues* [€/t <sub>RHW</sub> ]
Gasification	21	86	105	212	- 68
Pyrolysis	21	162	0	183	- 86



\*) Syngas @ 200 €/t  
Naphtha @ 500 €/t

\*\*\*) unit size ca. 100 MW / ca. 25 t/h  
of pretreated household waste (RDF)  
Capital investment cost estimate  
accuracy: ± 30%

# Feedstock Recycling of Waste



- Total cost for gasification as well as pyrolysis process chains range between 100 and 180 €/t for residual household waste
  - Products: Syngas (gasification) or Syncrude (pyrolysis)
  - Processing cost are most sensitive to capital investment
- Scalable processes competitive to incineration
  - Additional value by feedstock recycling
  - Waste / biomass co-processing
  - Contribution to circular economy

Economical attractiveness versus technology readiness

# Acknowledgements

IEA Bioenergy

Task 36

Integrating Energy Recovery into Solid  
Waste Management Systems

## Material and Energy Valorisation of Waste in a Circular Economy

**BKV** KUNSTSTOFF  
KONZEPTE  
VERWERTUNG

in cooperation with

**Plastics**Europe  
*Association of Plastics Manufacturers*